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In situ Investigation of Methane Dry Reforming on M-CeO$_2$(111) \{M= Co, Ni, Cu\} Surfaces: Metal-Support Interactions and the activation of C-H bonds at Low Temperature

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Abstract: Studies with a series of M-CeO$_2$(111) \{M= Co, Ni, Cu\} surfaces indicate that metal-oxide interactions can play a very important role for the activation of methane and its reforming with CO$_2$ at relatively low temperatures (600-700 K). Among the systems examined, Co-CeO$_2$(111) exhibits the best performance and Cu-CeO$_2$(111) has negligible activity. Experiments using ambient pressure XPS indicate that methane dissociates on Co-CeO$_2$(111), at temperatures as low as 300 K, generating CH$_x$ and CO$_x$ species on the catalyst surface. The results of density-functional calculations show a reduction in the methane activation barrier from 1.07 eV on Co(0001) to 0.87 eV on Co/CeO$_2$(111), and to only 0.05 eV on Co$_x$/CeO$_2$(111). At 700 K, under methane dry reforming conditions, CO$_2$ dissociates on the oxide surface and a catalytic cycle is established without coke deposition. A significant part of the CH$_x$ formed on the Co$_x$/CeO$_2$(111) catalyst recombines to yield ethane or ethylene.

Natural gas can transform the energy landscape of the world since it is a cheap and abundant fuel stock and a good source of carbon for the chemical industry. CH$_4$ is the primary component of natural gas but is difficult to convert it to upgraded fuels or chemicals due to the strength of the C-H bonds in the molecule (104 kcal/mol) and its non-polar nature.$^{[1]}$ Enabling low-temperature activation of methane is a major technological objective. It is known that enzymes such as the methane monooxygenase and some copper- and zinc-based inorganic compounds can activate C-H bonds near room temperature.$^{[2-4]}$ In recent studies, we found that a Ni$_{2+}$/CeO$_2$(111) system activates CH$_4$ at room temperature as a consequence of metal-support interactions.$^{[5,6]}$ The methane reforming with CO$_2$ (DRM; CH$_4$ + CO$_2$ → 2CO + 2H$_2$) then takes place at a moderate temperature of about 700 K. Over this surface, Ni and O sites of ceria work in a cooperative way during the dissociation of the first C-H bond in methane. Can this useful phenomenon be seen with other admetal-ceria combinations? In this article we compare the behavior of Co, Ni and Cu on CeO$_2$(111) using ambient-pressure X-ray photoelectron spectroscopy (AP-XPS), kinetic testing, and theoretical calculations based on density-functional theory.

The deposition of small amounts of Co (< 0.3 ML) on a CeO$_2$(111) film at 300 K produced a partial reduction of the oxide surface and adsorbed Co/CeO$_2$ species (Figure S1 in Supporting Information). Upon annealing from 300 to 700 K, most of the Co$^0$ transformed into Co$^{2+}$ (Figure S2). This particular type of metal-oxide surface was exposed to methane at 300, 500 and 700 K. Figure 1 shows C 1s XPS spectra collected before and after exposing a Co/CeO$_2$(111) surface to 1 Torr of methane at 300 K for 5 minutes. The strong peak near 285 eV can be attributed to CH$_x$ groups formed by the partial dissociation of methane on the metal/oxide interface.$^{[5,6]}$ This peak was not seen when a pure CeO$_2$(111) substrate was exposed to CH$_4$ at 300 K. In Figure 1 there is a second strong peak near 289.5 eV. This likely corresponds to a CO$_x$ species.$^{[5,6]}$ Some of the CH$_x$ molecules fully dissociated producing C atoms that eventually reacted with oxygen atoms of CO$_2$.
that found for clean CeO$_2$(111).\cite{5,6} In Figure 3, we compare the reduction of ceria (i.e. formation of Ce$^{3+}$) after dosing methane to Co-CeO$_2$(111), Figures S3 and S4, is not as strong as that seen for Co. The dissociation of methane on Cu/CeO$_2$(111) surfaces was negligible at temperatures between 300 and 700 K (Figure S5).

In this aspect, the behavior of these surfaces is very similar to that found for clean CeO$_2$(111).\cite{5,6} In Figure 3, we compare the reduction of ceria (i.e. formation of Ce$^{3+}$) after dosing methane to Co-CeO$_2$(111), Cu-CeO$_2$(111) and a Ni-CeO$_2$(111) system examined in a previous study.\cite{5} In the temperature range of 500-700 K, Co/CeO$_2$(111) reacts better with methane than Ni/CeO$_2$(111) or Cu/CeO$_2$(111). As we will see below, the partial reduction of ceria is important for the activation of CO$_2$ and closing the catalytic cycle for methane dry reforming.

In the case of Co/CeO$_2$(111), catalytic activity for methane dry reforming and C2 (ethane/ethylene) production was seen at 650 K (Figure 4). Clean CeO$_2$(111) did not display significant catalytic activity. However, the catalytic activity substantially increased when Co was added, reaching a maximum for the production of CO/H$_2$ at a coverage of ~0.15 ML. A maximum for the production of ethane/ethylene was seen at a Co coverage of 0.1 ML. At these small Co coverages, the Co/CeO$_2$(111) system had no problem dissociating CH$_4$ (Figures 1-3). The CH$_3$ groups generated on the surface underwent full decomposition to yield syngas or formed carbon-carbon bonds to produce ethane or ethylene. In Figure 4, the hydrogen is produced by methane dry reforming or by the generation of hydrocarbons (2CH$_4$ $\rightarrow$ C$_2$H$_6$/C$_2$H$_4$ + nH$_2$)\cite{7,8} CO and C$_2$H$_4$ also can be obtained through the reaction: 2CH$_4$ $\rightarrow$ 2CO + C$_2$H$_4$ + 2H$_2$O. At the maximum of catalytic activity in Figure 4, one can estimate a turnover frequency (TOF) of 6-7 molecules/Co atom $\cdot$ sec for methane dry reforming. At Co coverages above 0.2 ML, there was a steady decline in the catalytic activity. At the same time, postraction characterization of the catalysts with XPS showed an increase in the amount of atomic carbon present in the surface (Figure S6). This carbon could eventually lead to the formation of coke and catalyst deactivation. Thus, the optimum Co coverage is below 0.2 ML, when the interactions with the oxide support are important and the strength and number of the Co-Co interactions is limited.

In this study, we measured the catalytic activity of clean CeO$_2$(111) surface by exposure to 50 mTorr of CH$_4$ at different temperatures. Both ceria and Co$^{2+}$ species undergo reduction at 500-700 K as indicated by the emergence of Ce$^{3+}$ and Co$^0$ features. Once the first hydrogen is removed from the reactant molecule, a quick CH$_3$ $\rightarrow$ CH$_2$ $\rightarrow$ CH $\rightarrow$ C transformation occurs on the surface and oxygen atoms from the sample react to form CO and H$_2$O gas.
AP-XPS was used to study the chemical changes in the best Co/CeO$_2$(111) catalyst under reaction conditions. Figure 5 shows Ce 3d and Co 2p spectra collected while the catalyst is exposed to CH$_4$ or a mixture of CH$_4$/CO$_2$ at 700 K. Under pure methane one sees a surface with Co$^{2+}$ and strong peaks for Co$^{3+}$. The addition of CO$_2$ to the reactant gas leads to a weak reoxidation of Co and a substantial Ce$^{3+} \rightarrow$ Ce$^{4+}$ conversion. Two reaction paths are possible for the re-oxidation of the Ce$^{3+}$ in the support: CO$_2$(g) + Vac $\rightarrow$ CO(g) + O-oxide, or CO$_2$(g) + H(a) + Vac $\rightarrow$ HOCO(a) $\rightarrow$ HO-Vac + CO(g) and HO-Vac $\rightarrow$ O-oxide + H(a). Both of them could close the catalytic cycle for methane dry reforming after the process: CH$_4$(g) $\rightarrow$ C(a) + 4H(a); C(a) + O-oxide $\rightarrow$ CO(g) + Vac.

Figure 6 compares the catalytic activity for methane dry reforming of Co-, Cu- and Ni-CeO$_2$(111) clusters. The surface with Co is clearly the best catalyst, in agreement with the trends seen in Figure 3 for the activation of pure methane. Among these systems, Co-CeO$_2$(111) is the only one able to catalyze the 2CH$_4$ $\rightarrow$ C$_2$H$_2$ + (8-x)H$_2$ reaction (x = 4.6). The negligible catalytic activity of Cu/CeO$_2$(111) results from a very poor oxidation of CO$_2$, as indicated in Figure 3, which shows that reducibility increases in the order Cu $<$ Ni $<$ Co. In a set of experiments, we deposited small Co coverages (5-10 monolayers) and tested the catalytic activity for DRM in a flow reactor at temperatures between 700 and 975 K. The powder system did not show signs for deactivation and the conversion of methane through dry reforming was always close to that determined by equilibrium thermodynamics. These results are in agreement with the behaviour seen for Co/CeO$_2$(111) at 700 K.

Methane decomposition is frequently cited as the most difficult step for the DRM process. Here, we apply the spin-polarized DFT+U approach to investigate the dissociative adsorption of CH$_4$ on Co and Cu nanoparticles deposited on stoichiometric and reduced cerium oxide surfaces, plus the extended Co(0001), Co (111) and Cu(111) surfaces. Results will be compared to those recently obtained for Ni-ceria systems. The metal-ceria surfaces used for the experiments are quite complex. Co/CeO$_2$(111) displays high activity for methane dissociation at low metal coverages with Co atoms in close contact with the ceria support in a 2+ oxidation state, whereas Cu/CeO$_2$(111) is not active, with Cu$^{+}$ atoms aggregating to form larger metallic nanoparticles. Thus, we model these systems using single Co atoms and small tetrahedral Cu$_4$ clusters on CeO$_2$(111), Figure S7. We found that Co$^{2+}$ species (3d$^7$) adsorb most favorably at O-hollow sites in CeO$_2$(111), with the transfer of two electrons to the reducible support. Cu atoms transfer only one electron, yielding Cu$^{+}$ species (3d$^8$). The Cu$_4$ species also reduce the support, with the formation of two Ce$^{3+}$. The CeO$_2$(111) supported Co$_4$ and Cu$_4$ species behave similarly to the corresponding Ni$_4$ and Ni$_4$ ones. Moreover, low-loaded Co/CeO$_2$(111) with metallic cobalt, is the active phase for methane dry reforming, which will be modeled using single metal Co atoms on CeO$_2$(0001) (Figure S7). Hence, these M-ceria (M=Co, Cu) model surfaces mimic the essential features of the experimental catalysts as seen in the XPS data shown in Figures 3 and 5.

The molecular binding of methane to Co or Cu surfaces is very weak and dissociation, CH$_4$(a) $\rightarrow$ CH$_2$(a) + H(a), is difficult due to large energy barriers. Our calculated barriers are 1.07 and 1.64 eV (Figure S8), respectively, in agreement with previous studies. This is similar to Ni(111) with a barrier of about 0.9–1.1 eV. The molecular binding of CH$_4$ to Co$^{2+}$ and Cu$_4$ species on Co(111) lies within the 0.1-0.2 eV range (Figures 7a and S9). On the Cu/CoO$_2$(111) surface, similar to Cu(111), methane dissociation is hindered by a large energy barrier of 1.45 eV. This is consistent with the negligible methane dissociation observed for Cu-ceria systems at room temperature. Moreover, on Co/CeO$_2$(111), the barrier is reduced from 1.07 to 0.87 eV, as compared to Co(0001) (and from 1.02 eV if fcc Co(111) is considered, Figure S8). Therefore, the energy barrier for ceria supported small Co nanoparticles is accessible at lower temperatures than on the extended metal surface and methane dissociation is expected to occur, in agreement with the experiments shown in Figure 1. Here, metal and support work in a cooperative way in the dissociation of the C–H bond. Note that the final states shown in Figure 7a do not necessarily correspond to the lowest energy structures of the dissociated methane (Figure S9), but to local minima geometrically close to the transition state structures.

Upon increasing oxygen removal from the ceria support by reaction with methane, the Co$^{2+}$ species gradually recover their metallic state. Chemisorbed methane molecules on both M$^x$/CeO$_2$(0001) (M=Co, Ni) model systems are more stable than the corresponding M$^{2+}$/CeO$_2$(111) model systems (Figure 7), and thus the probability of reaction is expected to increase on the actual active dry reforming metal-CeO$_2$x catalysts. We observe that the distances between methane and the M$^x$/CeO$_2$(0001) (M=Co, Ni) surfaces, as measured by the C–M distances, are reduced by approx. 0.8 (Co) to 1.0 (Ni) Å with respect to the same distances in the M$^{2+}$/CeO$_2$(111) systems (Figures S9 and S10). Moreover, CH$_4$ adsorption on the M$^x$/
CeO₂(0001) surfaces is aided by substantial hydrogen-metal interactions that are more pronounced compared to the M²⁺/CeO₂(111) systems;

Figure 7. Reaction energy profile for the CH₄ → CH₃ + H reaction on: a) Cu, Co, and Ni on CeO₂(111) and b) Co, and Ni on CeO₂(0001). The activation barriers are hardly affected by inclusion of vdW interactions (Figure S14). The structures shown on the left, middle and right of the reaction pathways, correspond to the side views of the molecularly adsorbed, transition and cleaved. Therefore, more vacant sites and more Ce³⁺ ions are expected to form on Co-ceria catalysts as compared to Ni-ceria, in agreement with the experimental observations (Figure 3).

Our results on M-ceria (M=Co, Ni, Cu) model catalysts show that not only the nature of the metal is crucial for DRM activity and system stability, as recently pointed out for Ni, Co and Co-Ni nanoparticles, but also the oxide support can play an essential role. An oxide support can modify the electronic properties of an adsorbate in substantial ways making its chemical properties very different from those of the corresponding bulk metal. Single Co and Ni atoms on CeO₂ interact strongly with the reducible support while adopting a +2 oxidation state, and exhibit room temperature activity for C–H bond dissociation. Moreover, reducing the ceria support stabilizes metallic Co and Ni atoms and the systems are active for methane activation and dry reforming, with Co-CeO₂ being much more active than Ni-CeO₂. It is also seen that a low metal loading, below 0.2 ML, is crucial for the catalyst activity and stability since deactivation due to carbon deposition is observed at higher loading. This is consistent with the calculated trend in the adsorption energy of C atoms on the supported metal clusters of varying size (Figure S13), for example, Coₓ/Co-CeO₂ (-4.98/-4.12) < Co₄/Ni-CeO₂ (-6.86/-6.54 eV). Here, we show that by choosing the "right" metal-oxide combination and manipulating metal-oxide interactions, as well as controlling the effects of metal loading, an improved catalytic activity can be obtained. Our findings should be useful in the rational design of catalysts for reactions involving C–H bond dissociation. Cobalt-ceria can be added to the short list of oxide-based systems that can activate methane at room temperature, opening the possibility for new and exciting chemistry.

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Keywords: cobalt• ceria • methane dissociation • X-ray photoelectron spectroscopy • density functional theory

Low-loaded Co-CeO$_2$ is a highly efficient, stable and non-expensive catalyst for methane activation at RT and dry reforming at relative low temperatures (700 K), as revealed by experiments of ambient pressure XPS in combination with DFT calculations. Ethane/ethylene formation is also observed. Upon temperature increase the Co$^{2+}$/CeO$_2$ $\rightarrow$ Co$^{0}$/CeO$_{2x}$ transformation occurs, making the latter extremely active. The DRM activity strongly depends on the metal-ceria combination, with Co-ceria > Ni-ceria, and Cu-ceria being inactive.