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Food Hydrocolloids

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Highlights:

- Emulsifier type influenced the surface composition of powders
- The formulation containing conjugated WPH had the lowest powder stickiness
- Formulations containing lipid-based emulsifiers had the highest powder stickiness
- Conjugate-stabilised emulsions had the best quality upon reconstitution

Influence of emulsifier type on the spray-drying properties

2 of model infant formula emulsions

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23	Abstract
24	The objective of this study was to compare the drying performance and physicochemical
25	properties of model infant formula (IF) emulsions containing 43, 96, and 192 g L ⁻¹ protein,
26	oil and maltodextrin (MD), respectively, prepared using different emulsifier systems.
27	Emulsions were stabilised using either whey protein isolate (WPI), whey protein hydrolysate
28	(WPH; DH 8%), WPH+CITREM (9 g L ⁻¹), WPH+lecithin (5 g L ⁻¹) or WPH conjugated with
29	maltodextrin (DE 12) (WPH-MD). Homogenised emulsions had 32% solids content and oil
30	globules with mean volume diameter $<1~\mu m$. Powders were produced by spray-drying with
31	inlet and outlet temperatures of 170 and 90°C, respectively, to an average final moisture
32	content of 1.3%. The extent of powder build-up on the dryer wall increased in the order;
33	WPH - MD< <wph\subsection for="" observed="" same="" td="" the="" the<="" trend="" was="" wph+cit.="" wph+lec\subsection=""></wph\subsection>
34	extent of spontaneous primary powder agglomeration, as confirmed by particle size
35	distribution profiles and scanning electron micrographs, where the WPH-MD and WPH+CIT
36	powders displayed the least and greatest extent of agglomeration, respectively. Analysis of
37	elemental surface composition of the powders, showed that surface fat, protein and
38	carbohydrate decreased in the order; WPH+CIT>WPH+LEC>WPH>WPH – MD>WPI,
39	WPI>WPH>WPH - MD>WPH+LEC>WPH+CIT and WPH -
40	MD>WPI>WPH+LEC>WPH+CIT, respectively. Additionally, differences in
41	wettability, surface topography and oil globule distribution within the powder matrix and in
42	reconstituted powders were linked to the powder emulsifier system. Inclusion of the WPH-
43	MD conjugate in the formulation of IF powder significantly improved drying behaviour and
44	physicochemical properties of the resultant powder, as evidenced by lowest powder build-up
45	during drying and greatest emulsion quality on reconstitution, compared to the other model
46	formula systems.

- 47 **Keywords**: Spray-dried emulsions, Infant formula powders, Protein conjugation, Powder
- 48 stickiness, Emulsion stability, Particle microstructure



1. Introduction

49

50	Protein-based added-value nutritional formulations have been gaining a significant share of
51	the global food market over the last decade, especially those tailored for athletes, the elderly
52	and infants; the total global market for these product types is predicted to exceed 100 billion
53	USD by 2020. Formulations for such products generally contain protein (e.g., whey protein),
54	oils rich in unsaturated fatty acids (i.e., blends of vegetable oils) and carbohydrates (e.g.,
55	maltodextrin) as the main components. Whey protein hydrolysate (WPH) is often used as a
56	protein source in such nutritional formulae due to its desirable amino acid composition, high
57	digestibility and rapid absorption in the gut (Hernández-Ledesma, García-Nebot, Fernández-
58	Tomé, Amigo, & Recio, 2014). Modification of protein <i>via</i> hydrolysis has been extensively
59	studied, with reports on improvement in protein functionality in the areas of solubility,
60	surface activity, foaming and emulsifying properties available in the scientific literature
61	(Agboola & Dalgleish, 1996a, b; Banach, Lin, & Lamsal, 2013; Foegeding & Davis, 2011;
62	Kilara & Panyam, 2003). However, incorporation of WPH into nutritional formulations such
63	as powdered formulae or ready to drink products is often associated with processing and shelf
64	life challenges such as protein/peptide-mediated bridging flocculation and coalescence, due
65	to reduced steric stabilisation and increased number of exposed reactive sites, compared to
66	formulations based on intact whey protein (Drapala, Auty, Mulvihill, & O'Mahony, 2016a, b;
67	Euston, Finnigan, & Hirst, 2000; Hunt & Dalgleish, 1995). Irrespective of the format of the
68	final product (i.e., liquid or powder), the formulations for both physical formats have to
69	undergo a number of thermal treatments (e.g., pasteurisation, sterilisation, spray-drying) as a
70	liquid. Therefore, additional non-protein surface active components are often included in the
71	formulation of WPH-based emulsions in order to improve their processing and shelf-life
72	stability; these surfactants are usually lipid-based emulsifiers, including lecithin or citric acid
73	esters of mono- and di-glycerides (CITREM).

74	Spray-drying is one of the most common processes used in the manufacture of dairy
75	ingredients and nutritional products; rapid water removal results in increased product shelf-
76	life, reduced shipping and storage costs and provides the consumer with a convenient and
77	stable product. In this complex process, multiple factors such as feed characteristics (e.g.,
78	composition and rheological properties), process parameters (e.g., atomiser type and fines
79	return) and external factors (e.g., air humidity, temperature) significantly impact the drying
80	performance and the physicochemical properties of the final product. The composition (i.e.,
81	the type and content of protein, carbohydrate, fat and emulsifier, total solids content) and
82	properties (i.e., flow behaviour and viscosity) of the emulsion destined for spray-drying have
83	a strong influence on its drying properties; extensive scientific reports and reviews focusing
84	on the effects these factors have on the characteristics and properties of the resulting powders
85	have been published (Adhikari, Howes, Wood, & Bhandari, 2009; Jayasundera, Adhikari,
86	Aldred, & Ghandi, 2009; Ji et al., 2016; Kim, Chen, & Pearce, 2009; Millqvist-Fureby,
87	Elofsson, & Bergenståhl, 2001; Taneja, Ye, Jones, Archer, & Singh, 2013; Vega & Roos,
88	2006; Vignolles, Jeantet, Lopez, & Schuck, 2007).
89	It is well established that there is a strong relationship between the surface composition of
90	powder particles and their drying performance in addition to the properties (e.g.,
91	cohesiveness, shelf-life) of the final product (Kelly, O'Mahony, Kelly, & O'Callaghan, 2014;
92	Nijdam & Langrish, 2006; Sadek et al., 2015). In the production of fat-rich powders, high
93	surface fat content can lead to powder stickiness, low powder recovery (i.e., yield) and
94	production down-time (i.e., due to powder build-up on the dryer walls) as well as poor shelf
95	life and undesirable properties of the final product (i.e., lipid oxidation, caking, low solubility
96	and dispersibility) (Paterson, Zuo, Bronlund, & Chatterjee, 2007). Surface composition of an
97	emulsion-based powder is governed mainly by the emulsifier system used; upon atomisation,
98	a new air/liquid interface is created and surface active components (i.e., protein, peptides, low

99	molecular weight surfactants), present in the emulsion, migrate rapidly towards, and adsorb
100	at, the new interface, effectively reducing the surface free energy and enhancing the
101	thermodynamic stability of the system (Munoz-Ibanez et al., 2016). Effectively, surfactants
102	are over-represented at the droplet/powder particle surface, affecting in-process and in-
103	application behaviour of these products, as exhibited by interactions of particles with the
104	dryer wall and with other droplets/powder particles. Thus, a better understanding of the
105	emulsifier system and its modification to tailor it to a specific formulation has an important
106	role in increasing drying efficiency to produce a powder with desired properties.
107	Conjugation of milk proteins with carbohydrates through the Maillard reaction has been
108	frequently reported to give an emulsifier with exceptional functionality, especially with
109	respect to stability of emulsion to unfavourable thermal and/or storage conditions (Akhtar &
110	Dickinson, 2003; Drapala et al., 2016 a, b; Kasran, Cui, & Goff, 2013a, 2013b; O'Regan &
111	Mulvihill, 2010a 2010b; Wooster & Augustin, 2006). WPH-maltodextrin (WPH-MD)
112	conjugates have been shown to confer strong steric stabilisation to oil droplets, effectively
113	limiting globule-globule interactions and preventing emulsion destabilisation (i.e.,
114	flocculation and/or coalescence) (Corzo-Martínez et al., 2011; Liu, Ma, McClements, & Gao,
115	2016).
116	There is an evident potential for these conjugates to affect surface properties of spray dried
117	emulsions, effectively, influencing their behaviour during drying and properties of the final
118	product. Good interfacial barrier properties and inherent ability of WPH-MD conjugate to
119	adsorb at the newly formed air/water interface (O'Mahony, Drapala, Mulcahy, & Mulvihill,
120	2017) can offer an ingredient capable of deterring interactions between atomised emulsion
121	droplets/powder particles. However, currently there are no published studies reporting on the
122	use of WPH-based conjugates in spray dried emulsions nor on the properties of the resultant
123	powders. This study aims to directly compare the spray drying performance and powder

124	physical properties for spray dried emulsions stabilised with different emulsifier systems;
125	namely, conjugated protein/peptides (WPH), not conjugated protein/peptides (WPH, WPI)
126	and not conjugated protein/peptides (WPH) with the addition of low molecular weight lipid-
127	based surfactants (i.e., CITREM and lecithin).
128	2. Materials and methods
129	2.1. Materials
130	Whey protein isolate (WPI) and whey protein hydrolysate (WPH; 8% degree of hydrolysis;
131	DH) were obtained from Carbery Food Ingredients Ltd. (Ballineen, Co. Cork, Ireland). The
132	WPI and WPH ingredients had protein contents of 87.2 and 83.7%, respectively, and ash
133	contents of 2.76 and 2.92%, respectively, as reported by Drapala et al. (2016a). Maltodextrin
134	(MD) was obtained from Corcoran Chemicals Ltd. (Dublin, Ireland) and had moisture and
135	ash contents of <5.0% and <0.2%, respectively. Soybean oil was obtained from Frylite Group
136	Ltd. (Strabane, Co. Tyrone, Northern Ireland). CITREM (Grindsted® CITREM N12) was
137	obtained from Dupont Nutrition Biosciences ApS (Brabrand, Denmark) and de-oiled
138	powdered soybean lecithin (Ultralec® P) was obtained from ADM (Decatur, IL, USA). All
139	other chemicals and reagents used in the study were of analytical grade and sourced from
140	Sigma-Aldrich (Arklow, Co.Wicklow, Ireland).
141	2.2. Preparation of emulsions
142	Emulsions (e) for model infant formula (IF) powders (p) were prepared at pH 6.8 using
143	protein, soybean oil and maltodextrin in the ratios 1.0:2.3:4.5, respectively. The protein
144	component was either whey protein isolate (WPI), whey protein hydrolysate (WPH) or WPH
145	conjugated with maltodextrin (MD) in a wet heating process as detailed by Drapala et al.
146	(2016a). Additionally, non-protein emulsifiers, citric acid esters of mono- and di-glycerides
147	(CITREM; 9 g L ⁻¹) and soybean lecithin (5 g L ⁻¹) were incorporated into the formulation of

148	selected IF emulsions destined for subsequent spray-drying. Emulsions were prepared by
149	dissolving oil soluble components, where applicable, in soybean oil and water soluble
150	components in ultrapure water, followed by two stage homogenisation (double pass) at 15
151	and 3 MPa, using a valve homogeniser (APV GEA Niro-Soavi S.p.A., Parma, Italy) at 50°C.
152	All emulsions were prepared to a total solids (TS) target of 32% as measured with a rapid
153	moisture analyser (HB43 – S, Mettler – Toledo LLC, Columbus, OH, USA). In total, five
154	emulsions based on WPI, WPH, WPH + CITREM (WPH+CIT), WPH + lecithin
155	(WPH+LEC) and WPH conjugated with maltodextrin (WPH-MD) were produced in the
156	current study.
157	2.3. Spray-drying of emulsions
158	Powders were produced from emulsions using a bench-top spray dryer (B-191, BÜCHI
159	Labortechnik AG, Flawil, Switzerland) with a maximum evaporation capacity of $1.5\ L\ H_2O$
160	h ⁻¹ . Inlet temperature was set at 170°C and outlet temperature was maintained at 90-95°C by
161	controlling the aspirator power (i.e., in the range of 40-60 m ³ h ⁻¹) and the feed flow rate (i.e.,
162	in the range 1.2-1.4 L h ⁻¹). Effectively, drying temperatures were kept within the industry
163	relevant range typical for IF manufacture by using high feed flow rate (95-100%) and
164	relatively low aspirator power (80-90%); however, this was achieved at the expense of
165	product yield (Fig. 1). The powders were collected in the collection chamber as detailed in
166	Fig. 1, transferred to zip-sealed low density polyethylene bags (VWR International, Leuven,
167	Belgium), followed by vacuum packing in heat-sealed polyamide/polyethylene bags (Fispak
168	Ltd., Dublin, Ireland) with a moisture permeability of 2.6 g m ⁻² .d. The powders were stored
169	in the dark at ambient conditions (i.e., $\sim\!20^{\circ}\text{C}$) until further analyses within 4 weeks of spray
170	drying. Powder recovery was calculated on a TS basis (i.e., [Final powder product TS/feed
171	liquid TS] ×100) from the total amount of powder obtained in the collection chamber. Losses

172	on drying were due to unrecoverable powder, which stuck to the wall of the dryer main
173	chamber or fell and accumulated at the base of the main chamber during spray-drying (Fig.
174	1). Powder stickiness was visually assessed based on the extent of wall coating by powder in
175	the cyclone, in order to provide information on particle cohesion arising from surface
176	characteristics (Fig. 1).
177	2.4. Particle size distribution
178	Particle size distribution (PSD) of the emulsions immediately after homogenisation and after
179	powder reconstitution (i.e., 12%, w/v, TS) was measured using a laser light diffraction unit
180	(Mastersizer 3000, Malvern Instruments Ltd, Worcestershire, UK) equipped with a 300 RF
181	(reverse fourier) lens, an LED light source (λ of 470 nm) and a He-Ne laser (λ of 633 nm) as
182	detailed by Drapala et al. (2016b). The size distribution of the model infant formula powders
183	was measured using a Mastersizer 3000 equipped with a dry powder dispenser cell (Aero S).
184	Approximately 3.0 g of powder was placed in the feed hopper, containing a ball bearing to
185	facilitate powder flow, with the feed pressure set at 1 bar, powder flow rate at 40-70% and
186	the hopper height at 2 mm. All measurements were taken at 1-2% obscuration. The
187	background and sample measurement duration was set at 20 s with the material refractive and
188	absorption indexes of 1.46 and 0.01, respectively.
189	2.5. Rheological measurements
190	The apparent viscosity of emulsions was measured at 20°C using a rotational viscometer
191	(Haake RotoVisco 1, Thermo Fisher Scientific, MA, USA) equipped with a cylindrical
192	double gap cup and rotor (DG43, Thermo Fisher Scientific, MA, USA) as described by
193	Mulcahy, Mulvihill and O'Mahony (2016). The shear rate was increased from 0 to 300 s ⁻¹
194	over 5 min, held at 300 s ⁻¹ for 2 min and decreased to 0 s ⁻¹ over 5 min; the average apparent
195	viscosity was determined at 300 s ⁻¹ (η_{300}) for each emulsion. The power law of shear stress
196	(τ) versus shear rate (γ) was used to obtain flow curves and the flow behaviour parameters

197	consistency coefficient (K) and flow behaviour index (n) as detailed by Anema, Lowe, Lee,
198	and Klostermeyer (2014). The flow behaviour index (n) values are used to describe the flow
199	behaviour of liquid samples where $n < 1$, $n > 1$ and $n = 1$ indicate shear-thinning, shear-
200	thickening and Newtonian flow behaviour, respectively.
201	2.6. Composition and colour analyses of powders
202	The chemical composition of the model infant formula powders was determined using
203	standard International Dairy Federation (IDF) methods as detailed by Drapala, Auty,
204	Mulvihill, and O'Mahony (2015). Colour of the powders was measured using a pre-calibrated
205	colorimeter (Minolta Chroma Meter CR-400, Minolta Ltd., Milton Keynes, U.K.) equipped
206	with a granular-materials attachment CR-A50. Colour was expressed using the Commission
207	Internationale de l'Eclairage (CIE) colour chromaticity L* a* b* scale (L = dark/light, a =
208	red/green, b = yellow/blue).
208209	red/green, b = yellow/blue). 2.7. Powder wettability
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 209 210 211 212 213 214 215 	2.7. Powder wettability The sessile drop goniometric method was used to determine the wettability of powders. All powders were compressed for 10 s at 78.4 MPa using a manual press (15 ton Manual Hydraulic Press, Specac Ltd., Orpington, UK) to form pellets (13 mm diameter); all pellets had a density of 1.08 (\pm 0.05) g cm ⁻³ . Subsequently, the mean contact angle (θ) was determined directly using an optical tensiometer (Attension Theta, Biolin Scientific, Stockholm, Sweden); a drop (10 μ l) of ultrapure water was formed and deposited on top of a

219	2.8. Surface composition of powders
220	Surface free fat content of powders was determined using the GEA Niro analytical method
221	(GEA Niro, 2005) as described by McCarthy et al. (2013) with modified quantities of powder
222	(5.0 g), petroleum ether (30 mL) and filtrate (15 mL) used. Elemental composition of powder
223	surfaces was determined by X-ray photoelectron spectroscopy (XPS; Kratos Axis 165, Kratos
224	Analytical, UK) as detailed by McCarthy et al. (2013). A matrix formula was used to
225	calculate relative amounts of protein, fat and carbohydrate on the powder surface, as detailed
226	by Fäldt, Bergenståhl, and Carlsson (1993).
227	2.9. Microstructure of powders
228	2.9.1. Confocal laser scanning microscopy
229	Confocal laser scanning microscopy (CLSM) analysis of powder particles was performed
230	using a confocal laser scanning microscope (TCS SP, Leica Microsystems CMS GmbH,
231	Wetzlar, Germany). Powders were deposited onto a glass slide and excess sample was
232	removed with compressed air. The powder samples were stained with a mixture (3:1) of Nile
233	Red (0.10 g L^{-1} in polyethylene glycol) and Fast Green (0.01 g L^{-1} in water) fluorescent dyes
234	(Sigma Aldrich, Wicklow, Ireland) to label the fat and protein components of the powders,
235	respectively. Visualisation of oil and protein in the powders was carried out using an Ar laser
236	(excitation = 488 nm , emission = $500-530 \text{ nm}$) and He – Ne laser (excitation = 633 nm ,
237	emission = 650-700 nm), respectively. At least 3 representative images of each sample were
238	taken using $63 \times \text{ oil immersion objective.}$
239	2.9.2. Scanning electron microscopy
240	Scanning electron microscopy (SEM) analysis of powders was performed using a scanning
241	electron microscope (JSM – 5510, Jeol Ltd., Tokyo, Japan). Samples were mounted on
242	double-sided carbon tape, attached to SEM stubs, and then sputter-coated with
243	gold/palladium (10 nm; Emitech K550X, Ashford, UK). Representative micrographs were

244	taken at 5 kV at $1000 \times (i.e.$, overview of powder population) and $3000 \times (i.e.$, shape and
245	surface topography of powder particles) magnifications. At least three specimens of each
246	sample were observed to obtain representative micrographs of samples.
247	2.10. Statistical data analysis
248	All powders were prepared in three independent trials and all measurements were carried out
249	in at least duplicate. Analysis of variance (ANOVA) was carried out using the Minitab® 16
250	(Minitab Ltd., Coventry, UK, 2010) statistical analysis package. The Tuckey method was
251	used to obtain grouping information. The level of significance was determined at $P < 0.05$.
252	3. Results
253	3.1. Emulsion characteristics
254	The emulsions had TS levels ranging from 32.2 to 32.7% prior to spray-drying (Table 1).
255	Particle size analysis showed that all emulsions had oil globules with mean volume diameters
256	$(D_{4,3})$ less than 1 μm and no statistically-significant differences in $D_{4,3}$ were found between
257	the emulsions (Table 1). Similarly, no significant differences in the apparent viscosity (η_{300})
258	were observed between WPI _e , WPH _e , WPH+CIT _e and WPH+LEC _e emulsions; however, the
259	η_{300} for the WPH – MD_{e} emulsion was significantly lower than that of the WPI_{\text{e}}, and
260	WPH+CIT _e emulsions (Table 1). Analysis of the flow behaviour showed no significant
261	differences between emulsions, where most emulsions displayed a shear-thinning behaviour
262	(i.e., $n < 1$) (Table 1). A reduction in the viscosity during shearing (i.e., shear-thinning) of
263	protein solutions is, generally, a result of spatial rearrangement of protein molecules in the
264	liquid and of disruptions in their steady-state interactions (Walstra, Wouters, & Geurts,
265	2006); in emulsions, shear-thinning can be associated with flocculation of oil droplets (Xu,
266	Wang, Jiang, Yuan, & Gao, 2012). Additionally, in a concentrated emulsion system (i.e., TS
267	= 32%) packing of oil globules is denser than in a dilute emulsion (i.e. $TS < 12\%$) and

268	interactions between its constituents, as monitored by flow behaviour analysis, can be also
269	related to physical contact between molecules located at the interfaces of oil globules
270	(O'Mahony, et al., 2017). The formation of ternary complexes between unadsorbed
271	protein/peptides, CITREM and maltodextrin (Drapala et al., 2016b; Semenova, Myasoedova,
272	& Antipova, 2001) in the WPH+CIT _e emulsion, or the presence of intact whey protein in the
273	serum phase and at the interfaces of oil globules in the WPIe emulsion, is likely to have
274	contributed to higher viscosity of these emulsions, compared to the other samples.
275	3.2. Drying performance
276	Fig. 2 illustrates differences in drying behaviour between liquid concentrates/powders as
277	evidenced by different levels of wall-coating (i.e., multilayer particle cohesion) by fine
278	powder particles in the cyclone of the spray dryer. The extent of this coating is assumed to be
279	directly related to powder stickiness; the observed stickiness can be divided into 3 groups
280	based on the level of coating, i.e., non-sticky (negligible coating), moderately sticky (partial
281	coating) and very sticky (complete coating) (Fig. 2; Table 3). Using this classification, the
282	WPI_p and WPH_p powders were moderately sticky, $WPH+CIT_p$ and $WPH+LEC_p$ powders
283	were very sticky and the WPH-MD _p powder was non – sticky.
284	Differences in the stickiness of powders had a direct impact on the powder recovery (i.e.,
285	product yield; Table 3); the recovery of product was lower for products with higher level of
286	stickiness. Powders containing non-protein emulsifiers (WPH+LEC _p and WPH+CIT _p)
287	displayed the lowest powder recovery (18.1 and 21.3%, respectively) followed by WPI _p
288	(22.0%), WPH $_p$ (26.1%) and WPH-MD $_p$ (55.3%). It should be noted that in order to facilitate
289	the use of industry-relevant drying temperatures (i.e., 170°C and 90-95°C for inlet and outlet,
290	respectively) high feed flow rate (95-100%) and relatively low aspirator power (80-90%)
291	conditions were used. These conditions caused deposition of higher-moisture particles at the
292	periphery of the atomised feed jet on the inner wall of the main drying chamber (Fig. 1) and

293	contributed to the low powder yield. Sticking of powders to the inner wall of a spray dryer is
294	a common challenge in industry and it directly affects the product yield and drying efficiency
295	(i.e., cleaning and down-time). In high-fat powders (e.g., infant formulae) stickiness is
296	strongly related to the powder surface composition, while in low-fat, protein-dominant
297	powders, it is generally related to the efficiency of water removal and glass transition
298	properties of the system (Kelly et al., 2014). Generally, the more fat at the powder surface the
299	greater the challenges with powder stickiness (Sharma, Jana, & Chavan, 2012; Paterson et al.,
300	2007).
301	The highest levels of stickiness in this study were observed for powders containing lipid-
302	based emulsifiers (CITREM and lecithin) while the powder containing the protein-based
303	conjugate displayed the lowest stickiness. The physicochemical characteristics of CITREM
304	and lecithin have directly affected cohesiveness (i.e., stickiness) of powders; their high
305	mobility and surface activity facilitates rapid migration to the surface of emulsion droplets
306	formed on atomisation and their relatively low melting temperatures (55-65°C) make them
307	plastic and adhesive under the environmental conditions of spray-drying. Similarly, the
308	surface active WPH – MD conjugate can also rapidly move to and adsorb at the surface of
309	atomised droplets (O'Mahony et al., 2017).
310	3.3. Powder analyses
311	3.3.1. Composition and colour of powders
312	Compositional analysis of powders showed that the measured levels (Table 2) were in line
313	with the target levels for all samples (i.e., $12.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $56.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ protein, $26.9 - 29.0\%$ fat and $26.1 - 12.7\%$ for all $26.1 - 12.7\%$ for all $26.1 - 12.7\%$ for all $26.1 - 12.7\%$ fat and $26.1 - 12.7\%$ for all
314	58.8% carbohydrate). No significant differences were found in the fat, carbohydrate or
315	moisture content between the powders. No significant differences in colour were found
316	between WPI _p , WPH _p and WPH+CIT _p powders; these powders had high L* and low b*
317	values compared to the WPH-MD _p and WPH+LEC _p powders (Table 2). These differences

318	were most likely due to the presence of melanoidins (conjugation products) and carotenoids
319	(naturally present in lecithin) in the WPH-MD _p and WPH+LEC _p powders, respectively (Liu,
320	Ru, & Ding, 2012; McSweeney, 2008; Scholfield, 1981) as previously reported by Drapala et
321	al. (2016b).
322	3.3.2. Particle size distribution of powders
323	All powders had relatively small particles (i.e., $D_{4,3}$ of 14.2 – 41.1 μm ; Table 3). The biggest
324	particles were observed for the WPH+LEC _p , followed by the WPH+CIT _p , WPI _p , WPH _p and
325	WPH-MD _p powders (Table 3, Fig. 3B). In addition, powders containing lipid-based
326	surfactants, WPH+LEC _p and WPH+CIT _p , had a distinct shoulder on the higher end (i.e., at
327	\sim 100 μ m) of the size range, with a notable proportion of the particle population (i.e., 7.78 and
328	4.05%, respectively) in these powders having diameter $>$ 100 μ m (Fig. 3B; Table 3). A much
329	smaller shoulder was also present in the WPI _p and smaller still in the WPH _p powders (i.e.,
330	2.93 and 2.26% of particle population were >100 μm , respectively). The WPH-MD _p powder
331	had a monomodal profile with the narrowest size distribution, where the majority (i.e., ~99%)
332	of particles had diameters $<40~\mu m$ (Fig. 3B); this sample also had the largest proportion of
333	fine particles (i.e., 19.9% of total population had diameter $<$ 5 μm ; Table 3). The greater
334	proportion of small particles in the WPH-MD _p powder, compared to the other powders is
335	likely related to this liquid concentrate feed having the lowest viscosity of all samples
336	(Pisecky, 2012). Relationship between feed viscosity and the size of particles in the resultant
337	powder was also reported by Crowley, Gazi, Kelly, Huppertz, and O'Mahony (2014), where
338	increase in the particle size followed the increase in feed viscosity.
339	3.3.3. Powder wettability
340	The results for contact angle (θ) analysis showed that the highest θ was observed for
341	$WPH+CIT_p, \ followed \ by \ WPI_p > WPH+LEC_p > WPH-MD_p > WPH_p \ (Table \ 3). \ Generally,$
342	the more hydrophobic the surface (i.e., surface of powder pellet), the lower is its affinity for

343	interactions with water and, effectively, the higher the θ between the droplet of water placed
344	on that surface. Thus, the contact angle analysis is often used to study the affinity of powders
345	for interactions with water, providing information on powder wettability (i.e., lower θ =
346	better wettability). The differences in wettability between the WPI _p and WPH _p powders,
347	evidenced by different θ , were most likely directly related to differences in the physical state
348	of protein (i.e., native vs hydrolysed, respectively). Solubility is generally enhanced by
349	protein hydrolysis due to partial disruption of protein secondary and tertiary structure
350	resulting in increased water access and faster hydration in hydrolysed, compared with intact,
351	protein-based powders (Banach et al., 2013; Chobert, Bertrand-Harb, & Nicolas, 1988; Kelly,
352	O'Mahony, Kelly, & O'Callaghan, 2016; Panyam & Kilara, 1996). Longer wettability times
353	for model infant formula powders based on intact whey protein compared to partially
354	hydrolysed whey protein were reported previously by Murphy et al. (2015). Wettability of the
355	WPH-MD _p was similar to that observed for the WPH _p (Table 3). The better powder
356	wettability observed for the WPH+LEC _p , compared to the WPH+CIT _p , was likely due to the
357	differences in the nature of the two surfactants; CITREM and lecithin are anionic and
358	zwitterionic (i.e., amphoteric) surfactants, respectively (McSweeney 2008). Lecithin is often
359	coated onto the surface of the powders in a fluidised bed to facilitate improved solubility (i.e.,
360	instantisation) (Hammes, Englert, Zapata Norena, & Medeiros Cardozo, 2015).
361	3.3.4. Surface composition of powders
362	No significant differences were found in the free fat content for all powders due to large
363	standard deviations, especially observed for the WPH+LEC _p powder (Table 3). A trend was
364	observed, where free fat content was generally higher, for the WPH+CIT _p , WPH _p and
365	WPH+LEC _p powders (i.e., 20.0, 22.9 and 25.4%, w/w, free fat, respectively), compared to
366	the WPH-MD _p and WPI _p powders (i.e., 13.3 and 14.1%, w/w, free fat, respectively).

367	Table 3 shows differences in the surface composition (i.e., as measured using XPS) between
368	the spray-dried model IF powders prepared in this study. The level of protein at the surface
369	was highest for the WPI _p powder followed by WPH _p , WPH-MD _p , WPH+LEC _p and
370	WPH+CIT _p powders. The highest levels of surface fat were found in the WPH+CIT _p and
371	WPH+LEC _p powders. The amount of carbohydrate present at the surface was significantly
372	higher for the WPH-MD _p powder compared to the 2 powders containing lipid-based
373	surfactants (i.e., WPH+LEC _p and WPH+CIT _p).
374	The differences between the surface fat composition as measured by the solvent extraction
375	and by the XPS methods can be explained by the different principles underpinning these
376	methods. For the solvent extraction method the results are presented as the weight of
377	extractable fat as a % of the powder sample weight; conversely in the XPS method, the
378	results are presented as the % of surface area of the powder particle occupied by fat. For the
379	XPS method only a 10 nm depth of the surface of the powder particle is analysed (Kim,
380	Chen, & Pearce, 2009). Conversely, the solvent extraction approach extracts fat present at the
381	surface of the powder particle as well as fat present at other locations within its interior.
382	According to a model proposed by Buma (1971) the solvent-extractable free fat for dairy
383	powders consists of surface fat, outer layer fat from fat globules within the surface layer of
384	the particle, capillary fat constituted by fat globules that can be reached by the solvent
385	through capillary forces, and dissolution fat consisting of fat reached by solvent through holes
386	left by already extracted fat. A range of solvent extraction-based methods for assessment of
387	the amount of free or surface fat in spray-dried emulsions, reported in the scientific literature,
388	were compiled by Roos and Vega (2006) and it was shown that a these methods use different
389	solvent types (petroleum ether, hexane, pentane and carbon tetrachloride) solvent-to-powder
390	ratios $(5:1-40:1)$ and powder-solvent contact times $(30 \text{ s} - 48 \text{ h})$. The solvent extraction
391	method used in this study (GEA Niro, 2005) for quantification of the surface free fat in the

392	milk powders, with an extraction time of 15 min, could have led to the extraction of lipid
393	material in addition to surface fat alone (i.e., fat from the surface and from the interior of the
394	powder particles).
395	3.3.5. Microstructure of powders
396	3.3.5.1. Scanning electron microscopy
397	Fig. 4 A and B illustrate the detailed morphology (shape and structure) of the spray-dried
398	model IF powders. Differences between samples were mainly manifested by the extent of
399	particle agglomeration (i.e., spontaneous agglomeration of primary particles) and the
400	topography of the particle surfaces in the powders. Powders containing lipid-based
401	emulsifiers, WPH+CIT _p and WPH+LEC _p , displayed the greatest extent of particle
402	agglomeration, followed by WPI _p , WPH _p and WPH-MD _p (Fig. 4A). Such agglomeration is
403	generally caused by extensive particle cohesion (i.e., sticking) and is evidenced by the
404	presence of 'bunch of grape'-type agglomerates (Pisecky, 2012), as observed in this study for
405	the WPH+CIT $_p$, WPH+LEC $_p$ and, to a lesser extent, WPI $_p$ powders (Fig. 4A).). These
406	observations closely match the particle size distribution data discussed in Section 3.3.2. and
407	indicate cohesive interactions between particles during spray-drying.
408	The surface topography was also different between the powders; smooth surfaces were
409	observed for the WPI_p and to a lesser extent for $WPH\text{-}MD_p$ while the powder particles in the
410	WPH _p , WPH+CIT _p and WPH+LEC _p had an uneven surface with numerous bumps (WPH _p) or
411	craters (WPH+CIT _p and WPH+LEC _p) present on the surface (Fig. 4B). The presence of crater
412	- like structures on the surface of spray - dried emulsions/powders has been associated with
413	broken oil globules resulting in high levels of surface fat (Drusch & Berg, 2008).
414	Additionally, WPH – MD _p powder particles appeared to be partially collapsed (i.e.,
415	shrivelled) unlike particles in the other powders. Such shrivelled/buckled structures in spray-
416	dried powders has been linked with temperature-dependent changes in the volume of

417	occluded air (i.e., inflation followed by deflation of intra-particle air as the particle moves
418	from hot toward the cooler regions of the dryer) (Walton & Mumford, 1999) and with the
419	mechanical properties of the skin layer of the drying particles (Sadek et al., 2015, 2016).
420	3.3.5.1. Confocal laser scanning microscopy
421	Powders produced in the current study had generally similar particle structures, where
122	individual oil droplets were homogenously distributed within a protein-carbohydrate network
423	(Fig. 4C). The only exception was the WPH _p powder, where the oil phase appeared to be
124	largely present as irregular and extensive oil pools. Differences in the size of oil droplets
125	within the powder matrix were observed; powders containing lipid-based surfactants,
426	WPH+CIT $_p$ and WPH+LEC $_p$ had markedly bigger (2-3 μ m) oil droplets embedded in the
427	powder structure, compared to apparently smaller ($\leq 1~\mu m$) oil droplets in the WPI _p and
428	WPH-MD _p powders. Pools of oil or large oil droplets observed in CLSM micrographs can be
129	related to poor stability of these emulsions to processing. Additionally, 'empty' regions were
430	observed in the centre of the WPH-MD _p powder (Fig. 4C); these regions most likely indicate
431	the presence of internal air pockets (i.e., vacuoles) in particles of this powder as discussed in
432	Section 3.3.5.1. Formation of vacuoles and shrivelling of powder particles have been shown
433	to take place concomitantly (Sadek et al., 2015) and is strongly linked to the surface
434	composition of the droplet and, effectively, its drying kinetics (Nijdam & Langrish, 2006;
435	Vignolles et al., 2007).
436	3.3.6. Particle size distribution after reconstitution of powders
437	Notable differences were observed in the PSD between the reconstituted IF powders (Table
438	3; Fig. 3C); the mean volume diameter ($D_{4,3}$) and the value for the 90% quantile of the size
439	distribution ($D_{v,0.9}$) were higher for all reconstituted powders compared to the emulsions prior
440	to spray drying (Tables 1 and 3; Fig. 3A and C). The observed increases in $D_{4,3}$ and $D_{v,0.9}$
141	were most pronounced for the WPH, and WPH+CIT, powders (i.e. increases in D _{4.2} and

$D_{v,0.9}$ to $\geq 5 \mu m$ and $\geq 13 \mu m$, respectively); only a limited increase was observed for the
WPH-MD powder (i.e., $D_{4,3} < 1~\mu m$ and $D_{v,0.9} < 2~\mu m)$ (Table 3). The $D_{4,3}$ and $D_{v,0.9}$
parameters are particularly sensitive to changes at the large particle periphery of the size
distribution and their increase can be used as an indicator of associations between the larger
components in a system (i.e., coalescence and/or flocculation of oil globules in this case).
These differences reflect different stabilities of the corresponding formulations to the spray-
drying conditions (i.e., stability of oil globules against coalescence in a concentrated
emulsion system and stability to high heat and high shear stress in the atomiser chamber and
upon atomisation) and support the CLSM observations (see Section 3.3.5.1).

4. Discussion

The stability of emulsions to spray-drying was different for the studied formulations, as illustrated by the size distribution of oil globules in the powder matrix and in the reconstituted emulsions. These differences can be explained by the properties of the emulsifier systems used in these formulations, and their effect on stabilising emulsions against globule coalescence or heat-induced flocculation during processing. During spray-drying, emulsion-based systems are subjected to considerable stresses which can cause protein aggregation, breaking and coalescence of oil globules; this can lead to high surface free fat content and, effectively, undesirable properties of the resultant powder. Emulsions stabilised by high molecular weight (M_w) surfactants (e.g., protein) usually have thick and elastic interfacial films and are more stable to stress, compared to those stabilised by low M_w surfactants (e.g., CITREM, lecithin), which are prone to coalescence when forced in a close contact (Taneja et al., 2013). Formulations based on WPH often display poor thermal stability, due to exposure of reactive sites (e.g., free sulphydryl groups) at the surfaces of oil globules and in the bulk phase, often resulting in bridging flocculation of oil globules (Agboola, Singh, Munro, Dalgleish, & Singh, 1998; Drapala et al., 2016a). Such behaviour

467	was also reported in the current study, where oil pools in the WPH_p powder matrix and large
468	oil globules in this powder after reconstitution were present.
469	CITREM and lecithin are often added to improve thermal stability of WPH-based emulsions;
470	however, their presence can lead to competitive destabilisation, where protein/peptide-based
471	surfactants are displaced from the interfaces by smaller surfactants, promoting coalescence of
472	oil globules (Drapala et al., 2016a; Kaltsa, Paximada, Mandala, & Scholten, 2014; Mackie,
473	Gunning, Wilde, & Morris, 1999; Van Aken, 2003; Wilde, Mackie, Husband, Gunning, &
474	Morris, 2004). This was observed in the current study for CITREM- and lecithin-containing
475	powders, where large oil globules were observed in the powder matrix and in the
476	reconstituted emulsions (Fig. 4C, Table 3). In addition, topographical features observed for
477	samples containing lipid-based emulsifiers (i.e., craters; Fig. 4B) indicated that coalescence
478	of oil globules resulted in the presence of damaged oil globules at the powder surface
479	(Drusch & Berg, 2008). It is generally accepted that strong steric stabilisation of oil globules,
480	provided by protein-carbohydrate conjugates, can greatly limit these forms of destabilisation
481	(O'Mahony et al., 2017; Oliver, Melton, & Stanley, 2006). The presence of WPH-MD
482	conjugate in emulsions prevents interactions between individual oil globules and interactions
483	with bulk protein/peptides, resulting in enhanced stability. Results presented in the current
484	study show that superior stability of emulsions to spray-drying was achieved when the WPH-
485	MD conjugate was present in the formulation, compared to formulations containing CITREM
486	or lecithin.
487	In an emulsion, surface active molecules (e.g., protein, peptides, lecithin, CITREM,
488	conjugates) are adsorbed at the oil/water interface, where they stabilise oil globules; these
489	compounds are, generally, also abundant in the emulsion bulk phase as they are present in
490	excess of the concentration required for oil stabilisation. Upon atomisation, a new interface
491	(water/air) is formed at the surface of the atomised droplets and, during very short time

492	scales, surface active components move from the bulk to this new surface, adsorb and
493	rearrange (Munoz-Ibanez et al., 2016). Smaller surfactants move and adsorb faster due to
494	their higher mobility compared to large surfactants (Landstrom, Alsins, & Bergenstahl,
495	2000). Similar to the stabilisation of oil globules, the composition and structure of interfacial
496	layer of atomised droplets dictate their potential for interactions (i.e., stickiness,
497	agglomeration) (Nijdam & Langrish, 2006); in effect, surface composition and
498	physicochemical properties of the resulting powder are largely dependent on the surfactant
499	system of the emulsion. The high surface fat level observed for the WPH+CIT _p and
500	WPH+LEC _p powders and the high surface maltodextrin level observed for the WPH-MD _p
501	powder, could indicate preferential adsorption of lipid-based and conjugate-based
502	emulsifiers, respectively, at the surfaces of atomised droplets in these powders. Owing to the
503	different surface compositions, powders displayed different propensity for interactions
504	between individual atomised droplets/particles (i.e., primary spontaneous agglomeration) and
505	with the wall of the spray dryer (as measured by powder build-up in the cyclone). It is
506	generally recognised that high levels of surface free fat cause challenges with cohesive
507	interactions of powders (Jayasundera et al., 2009; Vega & Roos, 2006). Similarly, in the
508	current study, the likely preferential presence of lipid-based emulsifiers on the surface of
509	some of the powders may have contributed to greater cohesiveness and, effectively, could
510	have promoted agglomeration and powder build-up, compared to the other powders.
511	Properties of the feed and drying kinetics generally govern the shape of powder particles
512	(Walton & Mumford, 1999). Distinctive shrivelled particles observed for the WPH-MD _p
513	powder were likely related to significantly lower viscosity of that emulsion, compared to the
514	other emulsions (i.e., at the same TS content), effectively, impacting the rate of water
515	removal. Additionally, the more hydrophilic nature of the surface of atomised
516	droplets/powder particles for the WPH-MD _p system, resulting from higher surface

maltodextrin content, compared to the other samples could have promoted faster water
removal as evidenced by the lower moisture content of the resultant powder. According to a
study by Sheu and Rosenberg (1998), surface indentation for whey protein-based powders
was promoted by high drying rates, leading to wall solidification before the onset of particle
inflation. With progressive water removal during drying of a dairy-based system, a skin layer
is formed at the droplet surface and its properties further affect the kinetics of drying and the
final shape of the dried particles. Sadek et al. (2015) presented a model for mechanical
properties of skin layer of a droplet during drying, where, depending on protein type present
at the surface (i.e., whey protein or micellar casein), the mechanical properties of the skin
were different and affected the shape of the resultant dried particles. Those authors showed
that in casein micelle-dominant skins, the elastic modulus increased faster and the protein
skin reached the plasticity region earlier, producing shrivelled particles with ductile and
plastic skin, while it took longer for the whey protein-dominant skin to reach the plasticity
region, giving round particles with brittle and plastic skins. Particle indentation for whey
protein-based powders was reported to be linked to the ratio of protein to maltodextrin at the
surface of powder particles (Rosenberg & Young, 1993; Sheu & Rosenberg, 1998), where
surface indentation was inversely related to the proportion of whey protein in the particle
skin. In the study by Sheu and Rosenberg (1998), the authors showed that increasing the
maltodextrin proportion in the skin decreased its elasticity and, effectively led to the
formation of shrivelled powder particles. Such shrivelled morphology was observed in this
study for the WPH- MD_p powder particles. In addition, the presence of vacuoles observed in
the WPH-MD _p powder sample supports its fit to the model proposed by Sadek et al. (2015),
where vacuole formation and particle shrivelling were concomitant. With rapid water
removal from the atomised droplets during spray-drying, less latent heat energy is required
due to lower moisture content, and the energy (i.e., temperature) acting on the non-water

powder components is increased. This, effectively, can result in increased inflation of the droplet due to the expanding volume of air occluded within, followed by particle collapse (i.e., deflation) as the particles moves away from the heat source, resulting in a shrivelled hollow powder particle (Hecht & King, 2000; Walton & Mumford, 1999). The use of different emulsifier systems resulted in different surface composition of the resultant powders as well as different quality of reconstituted emulsions. It was demonstrated that the differences in powder surface composition influenced the kinetics of drying for these formulations and governed the cohesive interactions between atomised droplets/powder particles. Effectively, the presence of lipid-based emulsifiers (i.e., CITREM or lecithin) in formulations greatly increased the cohesive interactions resulting in extensive spontaneous primary agglomeration and, effectively, reduced product yield. On the other hand, when the conjugate-based emulsifier was present in the formulation, these cohesive interactions were markedly reduced.

5. Conclusions

The current study demonstrated that using the WPH-MD conjugate in the formulation of emulsion-based model IF powder improved its processing stability and affected the surface composition of resultant powder. The use of the conjugate in the formulation gave powder with decreased surface fat and increased surface carbohydrate levels, compared to systems containing lipid-based emulsifiers (i.e., CITREM or lecithin). In effect, conjugate-based powders displayed reduced cohesive behaviour, resulting in decreased agglomeration and markedly higher product yield; the opposite was observed for the powders containing lipid-based emulsifiers. This study showed that the surface composition of an emulsion-based powder and, effectively, its drying performance and final product characteristics were greatly improved by utilisation of interactions between the two components of the formulation (i.e., protein and carbohydrate). A significant potential was accentuated for conjugate-based

567	emulsifiers for applications in emulsion-based powders, where powder cohesion is a
568	challenge.
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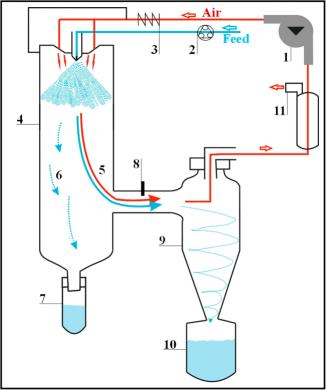
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Figure 1. Schematic diagram showing the set-up and the principle of operation for the laboratory-scale BÜCHI B-191 spray drier. The inlet temperature is regulated directly by the power of the heater (3) and the outlet temperature (measured at 8) is regulated indirectly by controlling the feed flow rate (2) and the air flow (1). Feed is introduced into the main drying chamber (4) by a 2-fluid nozzle atomiser, where it is rapidly dried by heated air; dried particles are pulled into the cyclone (9) by the means of an aspirator (1). Large and heavy particles (i.e., wet lumps and scorched particles, falling off the build-up around the nozzle and around hot air inlets, respectively) are separated from the powder by means of the air pull and gravity (5 and 6, respectively). By design, air pull is insufficient to move larger and heavier particles into the cyclone, making them fall into the waste collection container (7) at the bottom of the dryer main chamber. Dried powder particles are further separated from fines in the cyclone and the final powder is collected in the powder collection container (10) at the bottom of the cyclone. The clarified air is exhausted at the top of bag filter (11).

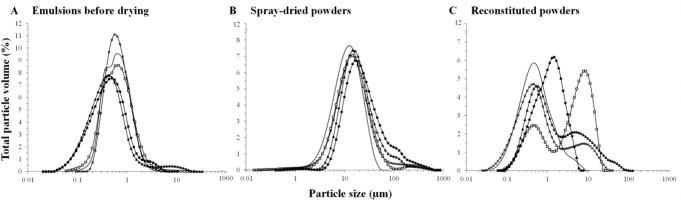
Figure 2. Differences in the build-up of fine powder on the wall of the cyclone during spraydrying of powders ($_p$) containing different emulsifier systems: whey protein isolate (WPI $_p$), whey protein hydrolysate (WPH $_p$), WPH + CITREM (WPH+CIT $_p$), WPH + lecithin (WPH+LEC $_p$) and WPH-maltodextrin conjugate (WPH-MD $_p$). The powders were produced using a laboratory-scale spray dryer (BÜCHI B-191). The photographs were taken ~30 min after starting the drying run for all powders.

Figure 3. Particle size distribution for (A) homogenised emulsions (dryer feeds), model infant formula powders (B) after spray-drying and (C) after powder reconstitution. The formulations contained different emulsifier systems: (\times) whey protein isolate, (\square) whey protein hydrolysate, (\triangle) WPH + CITREM, (\bullet) WPH + lecithin and (-) WPH-maltodextrin conjugate. The powders were produced using a laboratory-scale spray dryer (BÜCHI B-191).

Figure 4. Scanning electron microscope (SEM; A and B) and confocal laser scanning microscope (CLSM; C) images of model infant formula powders ($_p$) containing different emulsifier systems: whey protein isolate (WPI $_p$), whey protein hydrolysate (WPH $_p$), WPH + CITREM (WPH+CIT $_p$), WPH + lecithin (WPH+LEC $_p$) and WPH-maltodextrin conjugate (WPH-MD $_p$). For the CLSM analysis powders were labelled with Nile Red:Fast Green (3:1) and the micrographs show distribution of oil droplets (green) and protein particles (red). Scale bar for the CLSM micrographs = 5 μm. The powders were produced using a laboratory scale spray dryer (BÜCHI B-191).







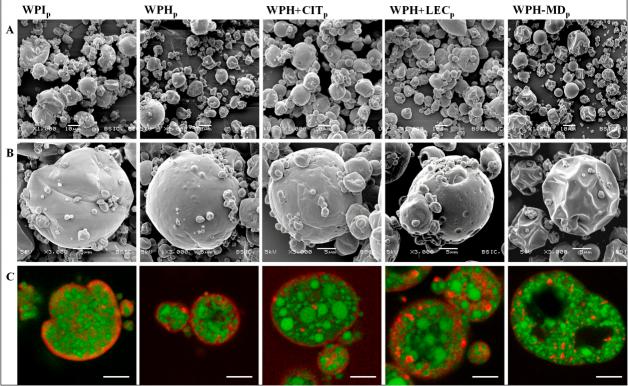




Table 1. Characteristics of emulsions prepared using different emulsifiers; whey protein isolate (WPI_e), whey protein hydrolysate (WPH_e), WPH + CITREM (WPH+CIT_e), WPH + lecithin (WPH+LEC_e) and WPH-maltodextrin conjugate (WPH-MD_e), used to produce model infant formula powders.

		Emulsions				
Emulsion characteristics		WPI _e	WPH _e	WPH+CIT _e	WPH+LEC _e	WPH – MD _e
Total solids content	(%, w/w)	32.6 ± 0.16^{a}	32.2 ± 0.69 a	32.5 ± 0.10^{a}	32.2 ± 0.04^{a}	32.7 ± 0.18^{a}
PSD¹ (μm)	$D_{4,3}$	0.76 ± 0.05^a	0.78 ± 0.14^{a}	0.81 ± 0.21^{a}	0.58 ± 0.06^a	0.67 ± 0.05^a
	$\overline{\mathrm{D}_{\mathrm{v,0.1}}}$	0.25 ± 0.07^{a}	0.21 ± 0.04^{a}	0.11 ± 0.07^{a}	0.15 ± 0.01^{a}	0.24 ± 0.05^{a}
	$\mathbf{D_{v,0.5}}$	0.55 ± 0.06^{a}	0.55 ± 0.01^{a}	0.38 ± 0.08^{a}	0.46 ± 0.12^{a}	0.55 ± 0.03^{a}
	$\mathbf{D_{v,0.9}}$	1.26 ± 0.10^{a}	1.40 ± 0.12^{a}	1.07 ± 0.07^{a}	1.52 ± 0.85^{a}	1.23 ± 0.04^{a}
Flow behaviour ²	η_{300} (mPa.s)	13.5 ± 0.55^{a}	11.9 ± 1.27^{ab}	13.0 ± 0.49^a	11.9 ± 0.24^{ab}	10.9 ± 0.31^{b}
	K (Pa.s ⁿ ; x10 ²)	1.57 ± 0.19^{a}	1.18 ± 0.22^{a}	2.92 ± 0.87^a	1.64 ± 1.25^{a}	2.19 ± 0.50^{a}
	n	0.97 ± 0.02^a	1.00 ± 0.02^a	0.85 ± 0.06^a	0.98 ± 0.16^a	0.87 ± 0.05^a

¹ Particle size distribution parameters: $D_{4,3}$, volume mean diameter of oil globules; $D_{v,0.1}$, $D_{v,0.5}$, and $D_{v,0.9}$ representing particle size in the 10%, 50% and 90% quantiles of the distribution.

² Flow behaviour parameters; (η_{300}) apparent viscosity measured at 300 s⁻¹; (K) consistency coefficient; (n) flow behaviour index.

⁽a-b) Values for a given parameter (i.e., within each row) for all powders, not sharing a common superscript differed significantly (P < 0.05).

Table 2. Composition and colour of model infant formula powders (_p) produced with different emulsifier systems: whey protein isolate (WPI_p), whey protein hydrolysate (WPH_p), WPH + CITREM (WPH+CIT_p), WPH + lecithin (WPH+LEC_p) and WPH-maltodextrin conjugate (WPH-MD_p). The powders were produced using a laboratory-scale spray dryer (BÜCHI B-191).

Powder	Composition	(%, w/w)		Colour coordinates				
	Protein	Fat	Carbohydrate	Ash	Moisture		a*	b*
WPIp	12.1 ± 0.21^{a}	28.4 ± 1.33^{a}	57.7 ± 0.99^{a}	0.52 ± 0.17^{a}	1.73 ± 0.35^{a}	96.1 ± 0.26^{a}	-1.26 ± 0.09 ^b	3.15 ± 0.24^{a}
WPH_p	12.6 ± 0.10^{b}	29.0 ± 1.58^{a}	56.1 ± 1.50^{a}	0.67 ± 0.10^{ab}	1.08 ± 0.66^{a}	96.3 ± 0.16^a	-1.30 ± 0.11^{b}	3.02 ± 0.15^{a}
WPH+CIT _p	12.3 ± 0.13^{ab}	28.8 ± 0.34^a	56.6 ± 0.43^a	0.87 ± 0.19^{ab}	1.36 ± 0.91^{a}	95.8 ± 0.49^{ab}	-1.26 ± 0.06^{b}	3.35 ± 0.26^a
WPH+LEC _p	12.7 ± 0.22^{b}	26.9 ± 2.44^a	58.2 ± 1.84^a	0.71 ± 0.13^{ab}	1.48 ± 0.34^a	93.8 ± 1.28^{c}	-1.96 ± 0.08^{a}	6.37 ± 0.25^{c}
WPH-MD _p	12.5 ± 0.09^b	26.9 ± 2.56^{a}	58.8 ± 3.17^{a}	0.97 ± 0.13^{b}	0.89 ± 0.34^a	94.1 ± 0.52^{bc}	-0.85 ± 0.07^{c}	4.77 ± 0.38^{b}

⁽a-c) Values for a given parameter (i.e., within each column) for all powders, not sharing a common superscript differed significantly (P < 0.05).

Table 3. Properties of spray dried model infant formula powders (p) prepared with different emulsifier systems: whey protein isolate (WPI_p), whey protein hydrolysate (WPH_p), WPH + CITREM (WPH+CIT_p), WPH + lecithin (WPH+LEC_p) and WPH-maltodextrin conjugate (WPH-MD_p). The powders were produced using a laboratory-scale spray dryer (BÜCHI B-191).

Powder characteristics		$\mathbf{WPI}_{\mathbf{p}}$	$\mathbf{WPH}_{\mathbf{p}}$	WPH+CIT _p	$\mathbf{WPH}\text{+}\mathbf{LEC}_{\mathbf{p}}$	WPH-MD _p
Drying performance ¹	Powder recovery (%)	22.0 ± 6.59^{a}	26.1 ± 3.27^{a}	21.3 ± 6.67^{a}	18.1 ± 2.56^{a}	55.3 ± 10.8^{b}
	Stickiness (relative)	+	+	++	++	
PSD (μm) Powders ²	$\mathbf{D}_{4,3}$	26.5 ± 16.9^{ab}	25.4 ± 4.79^{ab}	30.8 ± 2.94^{ab}	41.1 ± 13.2^{a}	14.2 ± 4.79^{b}
	$\mathbf{D}_{\mathrm{v},0.1}$	5.75 ± 0.56^{a}	5.85 ± 0.21^{a}	7.87 ± 0.54^{b}	9.52 ± 0.73^{c}	4.76 ± 0.27^{a}
	$\mathbf{D}_{\mathrm{v},0.5}$	15.5 ± 2.29^{ab}	15.1 ± 0.33^{ab}	18.4 ± 1.64^{bc}	22.7 ± 2.41^{c}	12.2 ± 0.94^{a}
	$\mathbf{D}_{\mathrm{v},0.9}$	59.5 ± 48.3^{a}	40.4 ± 3.22^{a}	56.0 ± 15.4^{a}	95.1 ± 43.6^{a}	26.6 ± 2.33^{a}
	% <5 μm	10.5 ± 2.16^{bc}	13.5 ± 0.71^{b}	$6.33 \pm 1.64^{\text{cd}}$	2.84 ± 0.81^{d}	19.9 ± 2.71^{a}
	% >100 μm	2.93 ± 6.92^{a}	2.26 ± 1.13^{a}	4.05 ± 0.93^{a}	7.78 ± 5.29^{a}	0.00 ± 0.00^{a}
Contact angle (θ)		42.1 ± 0.08^{b}	36.9 ± 1.45^{d}	46.7 ± 1.00^{a}	40.5 ± 2.27^{bc}	37.2 ± 0.91^{cd}
Surface free fat (%)		14.1 ± 2.68^{a}	22.9 ± 4.85^{a}	20.0 ± 5.05^{a}	25.4 ± 17.9^{a}	13.3 ± 1.18^{a}
Surface composition (%)	Protein	50.7 ± 6.42^{a}	37.1 ± 6.22^{b}	27.0 ± 2.81^{b}	29.1 ± 4.03^{b}	32.3 ± 2.02^{b}
	Fat	34.1 ± 9.42^{a}	50.9 ± 6.47^{ab}	64.2 ± 6.22^{b}	61.8 ± 6.82^{b}	50.0 ± 3.23^{ab}
	Carbohydrate	15.2 ± 3.02^{ab}	12.0 ± 0.91^{ab}	8.85 ± 3.50^{b}	9.12 ± 3.17^{b}	17.7 ± 1.61^{a}
PSD (μm) Reconstituted ²	D _{4,3}	2.42	5.72	5.00	1.47	0.84
	D _{v,0.1}	0.15	0.35	0.31	0.35	0.17
	D _{v,0.5}	0.57	4.68	1.10	1.18	0.51
	$\overline{D_{\mathrm{v},0.9}}$	8.02	13.3	14.4	3.07	1.82

¹ Drying performance describing powder recovery (%, w/w total solids, TS; powder TS/feed TS); stickiness classification: -, non-sticky; +, moderately sticky; ++, very sticky.

² Particle size distribution parameters: $D_{4,3}$, volume mean diameter; $D_{v,0.1}$, $D_{v,0.5}$, and $D_{v,0.9}$ representing particle size in the 10%, 50% and 90% quantiles of the distribution. Particle size distribution analysis for reconstituted powders was carried out only on one trial.

 $^{^{(}a-d)}$ Values for a given parameter (i.e., within each row) for all powders, not sharing a common superscript differed significantly (P < 0.05).